

# Long-term Durability of NO<sub>x</sub> Aftertreatment Systems for Diesel Engines

Lean NO<sub>x</sub> trap (LNT) systems are currently being improved in order to comply with the more stringent Tier 2 Bin 5 standards. Improving the LNT's durability is key in this endeavour. The main two aging mechanisms that need to be addressed are thermal deactivation and poisoning with sulphur. The two processes are linked because sulphur poisoning indirectly leads to thermal deactivation through regular desulfations of the catalyst. Those sulphur removal procedures expose the catalyst to considerable thermal stress that reduces its long term performance. Umicore research activities on improved LNT systems and data recorded in durability tests demonstrate substantially improved performance and durability. The main strategies employed were a reduction in the required desulfation temperature of the LNT as well as improved engine control and desulfation strategies.

# **1** Introduction

The main focus of powertrain development is shifting gradually to the improvement of fuel economy and the reduction of CO<sub>2</sub> emissions. Diesel vehicles are an important element in achieving those goals due to the good fuel economy of diesel cars compared to gasoline vehicles. Attractive fuel economy coupled with vastly improved performance of diesel cars have led to a passenger car market share of some 50 % in many European countries. In North America on the other hand the market penetration of diesel cars is still very low. Fuel economy hasn't been an important criterion for the consumer in the US due to low fuel prices. Furthermore the North American emission legislation does not grant less stringent standards to the diesel as it is the case in Europe. Therefore the North American standards, and in particular the NO<sub>2</sub>-standards are widely regarded as the most challenging ones anywhere in the world with respect to diesel cars. Rapidly increasing fuel prices in the US and an increased awareness of global warming has helped making a business case for the diesel in North America. Solving the technical challenges associated with the exhaust aftertreatment of diesel applications will be crucial to pave the way for a success of the diesel in North America.

The Mercedes-Benz E320 Bluetec represents the first North American diesel application which complies with the Tier 2 Bin 8 emission standards [1]. The key component that ensures adequate  $NO_x$  control is a  $NO_x$  storage catalyst, or lean  $NO_x$  trap (LNT). In order to increase robustness and reduce cost LNT systems are still being optimised and further improved. One main approach in that regard is a reduction of the required desul-

fation temperature necessary to remove the sulphur adsorbed on the catalyst which causes deactivation over time. The desulfation procedure involves quite harsh conditions of temperatures in the order of 600-750°C which can cause unwanted thermal deactivation of the catalyst. A lower propensity to adsorb sulphur as well as a lower desulfation temperature required to remove the sulphur lead to a substantially improved durability of the LNT.

In this paper we discuss a detailed study into the effect of thermal aging at different temperatures and for various periods of time. These data allow to precisely define optimal operating conditions which in turn ensure maximum long term performance of the catalyst. The main subject of the remainder of the text is a formulation, denoted catalyst A, that exhibits improved sulphur release properties that allows for lower desulfation temperatures and hence result in improved long term performance as demonstrated in engine bench testing.

# 2 Working Principle of the LNT

The basic mechanism of  $NO_x$  reduction by an LNT involves storage of  $NO_x$  under lean engine operating conditions and subsequent reduction to nitrogen in brief pulses of net reducing gas composition. Substantial improvement in engine calibration of diesel engines has led to very smooth lean/rich transitions that go completely unnoticed by the driver. The  $NO_x$  storage process involves the oxidation of NO, which is the most abundant  $NO_x$  species, to  $NO_2$ . This step is key since  $NO_2$  has a much higher adsorption rate than NO [2-5]:

 In the absorption process, NO<sub>2</sub> is stored as nitrate on basic sites on the

	1h	2h	5h	10h	20h	50h	100h
650°C			1	1	<i>✓</i>	1	1
750°C			✓	1	1	1	✓
800°C			1		1		
850°C	1		<ul> <li>✓</li> </ul>	1			
900°C	1	<i>✓</i>	✓				

Figure 1: Aging matrix containing aging temperature and duration

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Figure 2: NO $_{\rm x}$  conversion for different times of aging and two aging temperatures; left T=650°C, right T=750°C



Figure 3: NO $_{\rm x}$  conversion for different times of aging and two aging temperatures; left T=800°C, right T=850°C

tivity. Their thermodynamic stability decreases with increasing temperature and above 550°C Ba nitrates do not form anymore under lean gas atmosphere. The main storage materials comprise metal oxides that form stable nitrates in the relevant temperature range. Those are mainly oxides of alkali metals (Na, K, Rb, Cs), earth alkaline metals (Mg, Ca, Sr, Ba) and to some extend rare earth metals, like for instance La [2].

Two main mechanisms are responsible for the deactivation of an LNT catalyst in a diesel application [6-9]. Regular thermal regenerations of the particulate filter and desulfations of the LNT itself represent a substantial thermal load for the catalyst. Thermal aging impacts the NO<sub>2</sub> conversion activity at moderate operating temperatures between 150-350°C first, while NO<sub>v</sub> activity for higher operating temperatures is more resilient with respect to thermal exposure [8,9]. The second important deactivation mechanism involves the poisoning with sulphur contained in the exhaust gas. Sulfur forms very stable sulfates with the storage sites on the LNT and thereby reduces the number of sites available for NO\_storage. Sulfur removal involves exposing the catalyst to reducing conditions at elevated termperatures of some 600-750°C for several minutes. Desulfation intervals can be anywhere in the region of one thousand to several thousand km. Sulfur contained in the fuel is the major source of the poisoning agent SO<sub>2</sub> which is why low sulfur fuel with less than 10 ppm of sulfur is recom-

catalyst, mainly oxides of alkali or earth alkaline elements such as barium or potassium. The transformation from  $NO_2$  to nitrate involves another oxidation step which is belived to be assisted by precious metal present on the catalyst. The typical activity window of an LNT ranges from 150 to 500°C with a maximum  $NO_x$  conversion activity between 300 and 400°C.

In the temperature region below 300°C the activity is mainly limited by the kinetics of the NO-oxidation reaction. This reaction produces the precursor for the NO<sub>x</sub> storage, the NO<sub>2</sub>, and the rate of this reaction decreases with temperature. In the high temperature regime the stability of the nitrates limits the conversion ac-



Figure 4: NO, conversion for different times of aging at T=900°C



**Figure 5:** NO<sub>x</sub> conversion for different aging temperatures and given time of aging

mended in order to achieve realistic desulfation intervals. Low sulfur levels in the fuel reduce the numbers of desulfation events over the catalyst's lifetime and in turn reduce the thermal stress. Yet, even with 10 ppm of sulfur in the fuel the catalyst still needs to be desulfated regularly, albeit with longer mileage between two events. Since lubricants also contain some sulfur components, sulfur poisoning will most likely still be an issue even with possible increased future use of synthetic fuels.

A delicate balance has to be struck in choosing the optimal desulfation temperatures. The desulfation represents thermal stress which can impact the  $NO_x$  conversion activity at moderate temperatures below 300°C. On the other hand inefficient desulfation due to insufficient temperature levels causes  $NO_x$  conversion at higher operating temperatures above 400°C to suffer. The desulfation temperature must therefore be defined depending on the type of application and the temperature window where  $NO_x$  conversion activity is mostly required.

# **3 Aging Study**

A systematic aging study has been conducted by Umicore in order to assess the impact of high temperatures on catalyst aging. The discussion in this paper is mainly based on an advanced technology (catalyst A) which has been improved with respect to its sulfur release properties. Unless stated otherwise, the discussion always pertains to this particular

formulation. In the following sections of this paper, characterisation data comparing catalyst A with another formulation, catalyst B, will be discussed. Catalyst B exhibits a moderately higher desulfation temperature and an activity window shifted to slightly higher temperatures relative to catalyst A. The precious metal loading is 110g/cft in both cases. Both formulations contain only barium as a storage material. No other alkali or alkaline earth element is being used. The main difference of the two formulations is linked to the choice and processing of their constituent base metal oxides. In particular the question regarding the relative importance of aging temperature and duration was being investigated. The sensitivity of catalyst aging to both parameters is crucial in order to define the optimal window for operating conditions which at least partly results from the trade-off between required desulfation temperature and maximum acceptable thermal exposure.

Cores with dimensions of one inch diameter and 3 inch length were being aged in a furnace at different temperatures and exposition times, **Figure 1**. It contains systematically varying temperatures and aging durations in order to derive quantitative trends and assess the relative impact of temperature and exposure time. The aging temperatures were chosen in order to reflect relevant conditions on the vehicle. Shorter durations were chosen for the higher aging temperatures since long expositions are not realistic on the vehicle. Furthermore, since aging processes are faster at elevated temperatures and therefore happen on a shorter timescale. The aged samples were tested on a synthetic gas bench with respect to their  $NO_x$  conversion activity. The activity test involves monitoring the exhaust species under lean/rich cycling conditions, typical of the operation on the vehicle. The  $NO_x$  conversion values represent average numbers calculated by averaging over both the lean and rich cycle.

The duration of lean and rich cycles was 300 seconds and 20 seconds respectively at a space velocity of 35000/h. The NO<sub>v</sub> concentration was 100 ppm. Figures 2, 3 and 4 show the NO<sub>v</sub> conversion curve after aging for one given aging temperature and varying exposition time. Figure 5 finally shows a comparison for a constant expostion time and varying temperature. For the lowest aging temperature (650°C) there is no noticeable deactivation for any time between 5h und 100h of exposition. The slight spread of results is most likely due to statistical variations in the aging and testing procedures. For aging at 750°C the same is being observed as for 650°C aging. The exposition time seems to have no impact on NO<sub>x</sub> conversion activity for any duration between 5 and 100h (there are no data available for aging after 5h due to a malfunction of the analysis). For aging temperatures of 800, 850 and 900°C on the other hand there is a clear trend with exposition time. Longer thermal exposure leads to more severe deactivation of the catalyst.

Figure 5 compares the conversion curves for different aging temperatures with the fresh catalyst. Except for one



Figure 6: NO<sub>x</sub> conversions for two selected operating temperatures (200, 400°C) and two aging temperatures (left T=650°C, right T=750°C)

case, the catalysts were aged for 5 hours; only in the case of the 750°C aging the data for 10 hours aging were used since data for the 5h aging were not available. The plot shows that there are impacts of the aging for all temperatures even if an extension of the duration of the aging does not lead to further deactivation like in the case of 650 and 750°C. Thermal aging primarily affects NO, performance at lower temperatures, which is evident from the drop in activity at 150°C after 650°C aging. After aging 750°C there is also a reduction in NO<sub>v</sub> conversion activity at 200°C. For higher operating temperatures above 250°C however thermal aging causes an increase in the catalytic performance. This effect has already been described in the literature [2]. The reason is presumably linked to precious metal sites which have been shown to

limit the stability of nitrates at high temperatures. After moderate aging those precious metal sites sinter which attenuates their activity in general and their destabilising impact on nitrate sites in particular. Lower precious metal activity allows some nitrates to exist at higher temperatures than their inherent thermodynamic stability would suggest thereby improving  $NO_x$  storage at higher temperatures.

**Figure 6** shows  $NO_x$  conversion values for two operating temperatures (200 and 400°C) and two aging temperatures (650 und 750°C) plotted as a function of aging duration. Both aging temperatures cause an enhanced activity at 400°C because of the effect discussed above. On the other hand at 200°C operating temperature there is either virtually unchanged activity compared to the



Figure 7: Sulphur release rate as a function of temperature for catalysts A and B

fresh catalyst (for 650°C aging) or a clear deactivation of catalyst activity (for 750°C aging). In the future good performance at low exhaust temperatures becomes increasingly important, certainly for European applications.

One obvious strategy to protect low temperature NO<sub>v</sub> activity as much as possible is therefore a reduction of thermal exposure during desulfation events by improving the sulfur release properties of the catalyst. The catalysts technology discussed in the aging study (A) had been improved substantially with respect to the required desulfation temperature compared to its predecessor formulation (B). A reduction of the desulfation temperature by some 100°C allows to limit the peak thermal exposure during desulfation to 650°C and in turn to maintain good NO<sub>v</sub> conversion activity at moderate temperatures. Figure 7 shows lab results for sulfur release tests performed on synthetic gas bench for catalysts A and B. The plot shows the rate of sulfur release as a function of temperature. The peak of maximum rate of sulfur release is occurring at clearly lower temperatures for catalyst A compared to formulation B.

### 4 Engine Durability Testing

In order to assess the long term stability under more realistic operating contitions catalysts were aged on the engine bench and evaluated in regular intervals in simulated NEDC (New European Driving Cycle) tests. This work was being conducted in cooperation with Bosch. The investigations were carried out with a catalyst volume of 2.5 l on a 2.2 l common rail diesel engine. Diesel fuel with 50 ppm sulfur content was being used throughout, so this aging also included aging effects due to sulfur poisoning. The catalyst was desulfated in regular intervals (after 1g per litre of catalyst exposure) and its performance in the NEDC cycle was evaluated after each desulfation. An aging sequence was being conducted with technologies A und B using a desulfation temperature of ~750°C and a desulfation strategy which had been optimised for technology A, Figure 8. The NO<sub>v</sub> performance as evaluated in the NEDC drops from 95 % in



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**Figure 8:** NO<sub>x</sub> conversions as recorded on the engine bench in simulated NEDC driving cycles as a function of aging time. Vehicle mileage was extrapolated assuming 10 ppm sulphur fuel

the fresh state to some 60 % after 450 hours of aging. Based on the sulfur exposure and assuming typical fuel consumptions of low sulfur fuel (10 ppm) the entire aging corresponds to a mileage of some 200,000 km.

The trade off between the required desulfation temperature and the thermal aging linked to that is apparent in the test results. As Figure 7 shows the desulfation temperature for technology A is lower by some 100°C compared with catalyst B. The aging sequence was being repeated with catalyst A only and with a desulfation temperature of 650°C which is the optimal value for that technology. Furthermore the NO<sub>x</sub> regeneration strategy was being optimised. The results show an improved long term performance with a NO<sub>x</sub> conversion of some 85 % at the end of the aging.

## **5** Conclusions

A detailed aging study has been conducted by Umicore on synthetic gas bench in order to investigate the relative impact of aging temperature and

time of exposure. Both parameters have an important influence on the catalytic performance. At increasing temperatures the rate of thermal deactivation accelerates so that a maximum temperature limit should be defined that the catalyst is not to exceed. In the case of technology A this limit is somewhere in the region of 650-700°C in order to protect and maintain good performance in the regime of moderate temperatures of 200-250°C. A reduction of the desulfation temperature by increasing the rate of sulfur release is the most important strategy to achieve this goal. The aging tests on the diesel engine demonstrated the improved robustness and durability of technology A once the desulfation temperature is adjusted to the technology's optimal value. The present work shows that a wholistic approach is crucial for a successful implementation of an LNT in a diesel application. Targeted design of the the chemistry of the LNT formulation as well as a good understanding of the importance and influences of application parameters are key in order to ensure long term stability and robustness of the LNT system.